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Highlights

Turbulent entrainment in buoyant releases from horizontal gravity current to vertical planar wall plume

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- Study of the evolution of a two-dimensional, turbulent, miscible and steady gravity current and observation of the evolution of the layer using large-eddy simulations, with slopes varying from 0 to 90 degrees.
- The simulations showed three flow regimes. A regime for low angles in which the fluid transitions from the supercritical state to the critical state, a regime for intermediate angles associated with a fluid that remains inertial over its entire length and a regime for high angles in which the flow gains in inertia from the injection.
- In addition, a study of the entrainment for the each slopes revealed an increase with the slope until it reaches a constant value for a slope of 90 degrees, in accordance with the literature.
- Extension of the steady gravity current model introduced by Ellison & Turner (1959) for a non-Boussinesq configuration and highlighting of two specific theoretical angles: the critical angle θ_c , from which the mathematical singularity no longer appears, and the supercritical angle θ_{sc} , from which the fluid gains in inertia as soon as it is injected. These angles are associated with the different regimes observed in the numerical simulations.
- Development of a new entrainment law, including both the slope and the Richardson number, and comparison of the proposed law with those already in existence. In all the configurations discussed, the new law provides more reliable results than those found in the literature.

Turbulent entrainment in buoyant releases from horizontal gravity current to vertical planar wall plume

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Abstract

This paper examines the dynamics of a steady, miscible, two-dimensional gravity current flowing along an inclined boundary, with a particular focus on the entrainment, which refers to the mixing between the gravity current and the surrounding fluid. Specifically, the study investigates the combined effects of the Richardson number Ri and slope θ on the entrainment coefficient E . To address these objectives, large-eddy simulations (LES) were conducted, varying the slope angle from 0° to 90° , while maintaining constant injection conditions.

The simulations revealed three distinct flow regimes for our source conditions. The first regime, observed at low slopes ($\theta < 5^\circ$), exhibits a non-monotonic behavior, characterized by a transition from a supercritical to a subcritical regime. The second regime occurs at intermediate slopes ($5^\circ < \theta < 35^\circ$), where the flow remains inertial throughout. In the third regime, associated with steeper slopes ($\theta > 35^\circ$), the flow immediately gains inertia upon injection. The simulations also enabled an analysis of E , which was found to increase with slope and reach a constant value at $\theta = 90^\circ$.

A theoretical investigation of gravity currents was also conducted, resulting in the extension of the theoretical model of Ellison & Turner (1959) in the non-Boussinesq configuration as well as the identification of two specific angles: the critical angle θ_c , beyond which no mathematical singularity occurs, and the supercritical angle θ_{sc} , above which the flow acquires inertia immediately after injection.

Moreover, a new entrainment law was developed, incorporating both the effects of the Richardson number and the slope: $E = 0.002 \cos(\theta)/Ri + 0.09 \sin^{1/2}(\theta)$. This law provides a description of the entrainment behavior across the full range of slope angles. Comparisons between the LES results and the theoretical model demonstrate that the proposed entrainment law offers improved accuracy over existing models for all slope configurations, including the extreme cases of gravity currents ($\theta = 0^\circ$) and planar wall plumes ($\theta = 90^\circ$).

Keywords: gravity current, entrainment, slope, non-Boussinesq

1. Introduction

A gravity current is a flow driven horizontally by a difference between its own density and the density of its surroundings. This difference may result from distinct mechanisms such as a variation in temperature, salinity or concentration. The comprehension of this family of flows is of paramount importance for a better understanding of natural (Griffiths (1986), Dufek (2016))

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6 or industrial (Hoult (1972)) processes. Typically, gravity currents propagate along a boundary,
7 which may be inclined or horizontal. Alternatively, it can develop between two layers of fluids
8 of different densities. In this configuration, which will not be discussed in the present paper, the
9 current is known as an intrusion (Flynn & Linden (2006)).

10 Gravity currents are complex flows and are commonly studied for two configurations. The
11 first configuration, known as the "lock-exchange", involves an initially fixed volume of fluid
12 being released into an environment of different density (Shin et al. (2004)). This unsteady set-
13 up allows the investigation of several phenomena such as the velocity of the front (Rottman &
14 Simpson (1983)) or the influence of the wall on the propagation (Nogueira et al. (2013)).

15 The second configuration corresponds to a continuous release of the current from a nozzle.
16 In this set-up, the unsteady state of the flow can also be studied. For example, Hogg & Woods
17 (2001) work on the influence of the drag on the propagation velocity, Sher & Woods (2017) deal
18 with the entrainment of the head and Martin et al. (2020) study the influence of the slope. In
19 contrast to the lock-exchange setup, this configuration enables the observation of a steady-state,
20 enabling to model the flow using "top-hat" variables, akin to the models developed for plumes
21 by Morton et al. (1956) and for gravity currents by Ellison & Turner (1959).

22 In their pioneering work, these latter authors proposed a theoretical model based on the con-
23 servation equations for mass, momentum, and energy. This theoretical model yields a system of
24 coupled ordinary differential equations, which describe the streamwise evolution of the top-hat
25 velocity U , the top-hat density ρ and the thickness h of the current. These equations introduce
26 the Richardson number, corresponding to the ratio between the buoyancy and inertia forces, and
27 defined as follows : $Ri = \Delta\rho g h / \rho_a U^2$ (with $\Delta\rho = |\rho - \rho_a|$, ρ_a being the density of the ambient
28 and g the gravitational acceleration). The Richardson number is also used to characterize the
29 flow by defining three regimes: supercritical when $Ri < 1$ (momentum-dominated), sub-critical
30 when $Ri > 1$ (buoyancy-dominated) and critical when $Ri = 1$.

31 Inherent in their model, Ellison & Turner (1959) particularly address the issue of local en-
32 trainment. This phenomenon, which occurs when fluids are miscible, corresponds to the mixing
33 between the fluid and its environment. Using a small-scale experiment, these authors identified
34 a dependency between the Richardson number and the entrainment coefficient E expressed as
35 $E \propto Ri^{-1}$. Furthermore, Ellison & Turner (1959) suggest that entrainment becomes negligible
36 when $Ri > 0.8$. Later, Turner (1986) provides the mathematical relation associated with these
37 results:

$$E = \frac{0.08 - 0.1 Ri}{1 + 5 Ri} \quad \text{for } Ri < 0.8. \quad (1)$$

38 The work of Ellison & Turner (1959) became the foundation for many subsequent studies,
39 partially compiled in Fernando (1991), which were aimed at refining the modelling of the local
40 entrainment coefficient E . The majority of these works support the relation between the Richard-
41 son number and the entrainment coefficient initially proposed by Ellison & Turner (1959) (Parker
42 et al. (1986), Johnson & Hogg (2013)). However, some researchers argue that entrainment per-
43 sists even when the Richardson number exceeds unity (Lofquist (1960), Princevac et al. (2005)),
44 while others contend that a single governing law cannot describe the entire range of Richardson
45 numbers (Christodoulou (1986)). Additionally, certain models incorporate further parameters,
46 such as a flux coefficient (Wells & Wettlaufer (2005)) or the Reynolds number (Cenedese &
47 Adduce (2010)).

48 The study by Ellison & Turner (1959) also covers the entrainment with a slope of 90° (similar
49 to a planar wall plume bounded by a vertical surface). In this configuration, the authors use a

50 global entrainment coefficient E_{global} calculated from the difference between the inlet and outlet
 51 mass flow rates to quantify the amount of fluid entrained. Ellison & Turner (1959) obtained
 52 a constant entrainment coefficient equal to $E_{\text{global}} = 0.087$. They report that this result is in
 53 agreement with the value of 0.075 observed for a jet, while being in the same range as the result
 54 provided by Morton et al. (1956) in their seminal work on the modeling of an axisymmetric
 55 plume ($E = 0.1$).

56 In the specific case where the slope angle is 90° , Grella & Faeth (1975) conducted experi-
 57 ments that included the effects of heat transfer to investigate the influence of the wall on local
 58 entrainment. They found $E = 0.095$, which closely matches the value recently found by Zúñiga
 59 et al. (2024) through direct numerical simulations (DNS). The magnitude of these findings is fur-
 60 ther supported by the freshwater/saltwater experiments conducted by Parker et al. (2020), where
 61 $E = 0.08$. Additional experimental investigations (Lai & Faeth (1987), Sangras et al. (2000))
 62 and DNS simulations (Georges et al. (2021)) corroborate these results, suggesting that the en-
 63 trainment coefficient for a top-hat planar wall plume (or gravity current inclined at 90°) is close
 64 to 0.09.

65 Finally, Ellison & Turner (1959) also reported results for global entrainment at varying slope
 66 angles. The authors observe an increase in entrainment with increasing inclination. The subse-
 67 quent literature provides less detail on the inclined configuration. Britter & Linden (1980), from
 68 visual observations, present quantitative values of the entrainment with a slope. Although direct
 69 comparison with the data from Ellison & Turner (1959) was not possible due to differences in
 70 post-processing methods (Ellison & Turner (1959) is based on the top-hat height and Britter &
 71 Linden (1980) is based on the visual thickness of the flow), the trend of increased entrainment
 72 with slope was confirmed. Pawlak & Armi (2000), on their side, found significantly larger en-
 73 trainment values than those reported by Ellison & Turner (1959) for slopes less than 15° . Zúñiga
 74 et al. (2024) also dealt with this issue by performing DNS simulations at different angles. They
 75 observed a thickening of the current, and came to the same conclusions as Ellison & Turner
 76 (1959), with an increase in entrainment as the slope increases, until it becomes constant for steep
 77 slopes ($\theta > 61^\circ$). Several other authors have proposed angle-dependent entrainment laws, which
 78 are summarized in table 1.

79 The majority of these laws are solely dependent on the slope angle, assuming a constant
 80 entrainment coefficient for a given angle regardless of the Richardson number. This is in agree-
 81 ment with the literature for angles near 90° . However, for smaller angles, the influence of the

Reference	Law	Remarks
Pedersen (1980)	$0.072 \sin(\theta)$	-
Briggs (1980)	$0.05 \sin(\theta)^{2/3}$	-
Hopfinger (1983)	$9.5 \times 10^{-4}(\theta + 5)$	Law based on Ellison & Turner (1959)
Hopfinger (1983)	$4 \times 10^{-3}\theta$	Law based on Britter & Linden (1980)
Wells & Wettlaufer (2005)	$E_p \sin(\theta)$	$\theta > 5^\circ$
Hughes & Griffiths (2006)	$0.1 \sin(\theta)$	$\theta > 5^\circ$
Salinas et al. (2022)	$\frac{Ri \tan(\theta) - C_d}{C}$	$0.14^\circ < \theta < 2.86^\circ$

Table 1: Entrainment laws from the literature including an angle.

82 Richardson number on the entrainment could be questioned. The only law combining these two
83 parameters is the one suggested by Salinas et al. (2022), but it is restricted to very low slopes
84 ($0.14^\circ < \theta < 2.86^\circ$).

85 The question that now arises, and which we will attempt to answer throughout this paper, is
86 the following: Is it possible to establish an entrainment law that accounts for both the Richardson
87 number and slope angle in order to respect the observations made in the literature for slopes
88 varying between 0° and 90° ? Such a law requires us to observe the local evolution of the
89 current, in contrast to the law given by Ellison & Turner (1959), which is based exclusively on
90 global quantities.

91 To answer this question, our investigation proceeds in several stages. Firstly, to investigate
92 the physics of these flows, section 2 describes the large-eddy simulations carried out for slopes
93 ranging from 0 to 90° . These simulations are then post-processed to extract local information
94 on the top-hat variables as well as the entrainment. In section 3, the theoretical aspects of the
95 current are studied, in particular the influence of slope on the equations, and we develop a new
96 entrainment model based both on the simulation results and the literature. This entrainment
97 model is then challenged in section 4 before finally drawing conclusions in the last section of the
98 paper.

99 2. Numerical simulations

100 To simulate a non-Boussinesq turbulent miscible gravity current, we consider an isothermal
101 and continuous release of an air-helium mixture along an inclined boundary within a denser
102 ambient environment. In the set of eight simulations carried out, the velocity and the density of
103 the flow at the source are fixed at $u_0 = 1.3$ m/s and $\rho_0 = 1$ kg/m³, respectively. The source height
104 remains constant either and is set to $h_0 = 0.2$ m. The ratio between the density of the injected
105 fluid and the ambient fluid is $\rho_0/\rho_a = 0.914$ (weakly non-Boussinesq). Under these source
106 conditions, the Richardson and Reynolds ($Re_0 = u_0 h_0/\nu$, where ν is the kinematic viscosity)
107 numbers are respectively 0.237 and 14 000. The only variable parameter is the tilt angle θ , and
108 the set of simulations performed is shown in table 2.

109 We use large-eddy simulations (LES) to solve the Favre-filtered mass and momentum bal-
110 ance, using the numerical computational code CALIF³S. This software, developed at the French

	u_0 (m/s)	ρ_0 (kg/m ³)	h_0 (m)	Ri_0	Re_0	θ (°)	L (m)
Case 0	1.3	1	0.2	0.237	14 000	0	9
Case 1	1.3	1	0.2	0.237	14 000	5	9
Case 2	1.3	1	0.2	0.237	14 000	11	9
Case 3	1.3	1	0.2	0.237	14 000	19	9
Case 4	1.3	1	0.2	0.237	14 000	35	9
Case 5	1.3	1	0.2	0.237	14 000	56	9
Case 6	1.3	1	0.2	0.237	14 000	77	9
Case 7	1.3	1	0.2	0.237	14 000	90	9

Table 2: Source conditions, Richardson number, Reynolds number, slope angle, and length of the domain of the simulations carried out.

111 Institut de Radioprotection et de Sûreté Nucléaire (IRSN), is specifically designed for three-
 112 dimensional simulations of turbulent and slightly compressible flows. The three-dimensional
 113 (index i) filtered Navier-Stokes equations are:

$$\frac{\partial \bar{p}}{\partial t} + \frac{\partial(\bar{\rho}\bar{u}_i)}{\partial x_i} = 0, \quad (2)$$

$$\frac{\partial(\bar{\rho}\bar{u}_i)}{\partial t} + \frac{\partial(\bar{\rho}\bar{u}_i\bar{u}_j)}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial \bar{S}_{ij}}{\partial x_j} + (\rho_a - \bar{\rho})g_\theta - \frac{\partial \tau_{ij}}{\partial x_j}, \quad (3)$$

114 where \bar{u}_i represents the Favre-filtered velocity and \bar{p} denotes the dynamic pressure. $\bar{\rho}$ is the
 115 filtered density of the fluid and is computed using the ideal gas law and the mass fractions
 116 of the different species in the gas mixture. In equation (3), $g_\theta = g \cos(\theta)$ correspond to the
 117 gravitational acceleration, $\tau_{ij} = \bar{\rho}\bar{u}_i\bar{u}_j - \bar{\rho}\bar{u}_i\bar{u}_j$ is the subgrid-scale Reynolds stress, and $\bar{S}_{ij} =$
 118 $-(2/3)\mu(\partial\bar{u}_k/\partial x_k)\delta_{ij} + \mu(\partial\bar{u}_i/\partial x_j + \partial\bar{u}_j/\partial x_i)$ represents the filtered strain rate tensor and μ is the
 119 dynamic molecular viscosity.

120 The mass fraction y_k for each species k is determined through the transport equation for
 121 species:

$$\frac{\partial \bar{\rho}\bar{y}_k}{\partial t} + \frac{\partial(\bar{\rho}\bar{y}_k\bar{u}_i)}{\partial x_i} = \frac{\partial}{\partial x_i} \left(\bar{\rho}D \frac{\partial \bar{y}_k}{\partial x_i} + \frac{\mu_t}{Sc_t} \frac{\partial \bar{y}_k}{\partial x_i} \right), \quad (4)$$

122 where \bar{y}_k is the Favre-filtered mass fraction of the k -th component of the mixture, and D is
 123 the molecular diffusivity of the mixture. The closure of the problem is achieved by setting the
 124 turbulent Schmidt number Sc_t to 0.7, following the simple gradient diffusion hypothesis (SGDH).
 125 The code has already been used and validated to study flows characterised by small or large
 126 density differences, such as gravity currents (Haddad et al. (2022)), heavy and light discharges
 127 such as jets (Salizzoni et al. (2023), Salizzoni et al. (2024)) and fountains (Vaux et al. (2019)).

128 In our large-eddy simulations, we adopt the wall adapting local eddy subgrid-scale model
 129 (WALE, Nicoud & Ducros (1999)) for the subgrid Reynolds stress and we apply a box filter
 130 in each direction. A staggered grid with a cell-centred piecewise constant representation of the
 131 scalar variables is used as well as a marker and cell (MAC) type finite volume approximation for
 132 the velocity. The time discretization is done with a fractional step algorithm decoupling balance
 133 equations for the transport of species and Navier-Stokes equations. These latter are solved by a
 134 pressure correction technique.

135 The computational domain Ω is a rectangular box of dimensions $L_x \times L_y \times L_z$. The horizontal
 136 length is $L_x = L_0 + L$ (where L_0 is the position of the injection and is equal to $5h_0$). The vertical
 137 length L_z is equal to $20h_0$ and the spanwise width L_y is equal to $6h_0$.

138 In the horizontal streamwise direction of Ω , the mesh is divided into two zones: the first
 139 extends from $x = 0$ to the injection position $x_i = L_0$ and the second from the injection position
 140 to the outlet position at L_x . In the first zone, a uniform Cartesian rectangular mesh ($\Delta x_1 \times \Delta y$) is
 141 used. The grid is refined in the second zone with a uniform rectangular mesh ($\Delta x_2 \times \Delta y$).

142 In the vertical direction (z), the grid spacing Δz is kept constant from the ceiling to the in-
 143 jection height i.e. $z = h_0$ (with $\Delta z = \Delta z_1$), still uniform from $z = h_0$ up to a vertical distance
 144 L_{1z} corresponding approximately to the boundary of the current. Beyond this region, the grid is
 145 further stretched until it reaches the bottom of the domain.

146 For each case, we performed a grid-convergence study to validate the extent of the vertical
 147 subregion L_{1z} and the grid resolution in each direction. We tested vertical grid spacings $\Delta z_1/h_0$
 148 ranging from 0.1 to 0.05 and $\Delta z_2/h_0$ ranging from 0.15 to 0.075, horizontal grid spacings $\Delta x_1/h_0$

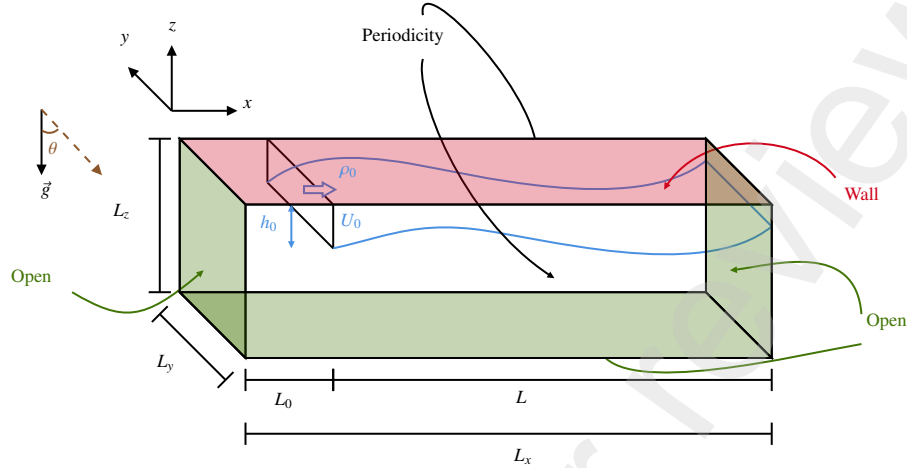


Figure 1: Representation of the computational domain Ω with the boundary conditions associated to the border of this domain.

149 from 0.15 to 0.075 and $\Delta x_2/h_0$ from 0.1 to 0.06 and finally spanwise grid spacing $\Delta y/h_0$
 150 from 0.15 to 0.05. For the time discretization, we impose a Courant-Friedrichs-Lewy number
 151 close to unity even if time step sizes for which CFL numbers greater than one are allowed with
 152 implicit schemes.

153 Given that the modeled flow propagates in an infinite (open) environment, it is necessary to
 154 bound the computational domain Ω with artificial boundary conditions, as illustrated in figure 1.
 155 For the left, bottom and right boundaries, we apply a boundary condition based on the usual control
 156 of the kinetic energy, which allows us to distinguish between the flow that enters the domain
 157 and the flow that leaves. This type of condition was originally formulated for incompressible
 158 flows in Bruneau & Fabrie (1994) and in Bruneau & Fabrie (1996), and its extension to compressible
 159 flows was tackled in Bruneau (2000). In addition, periodic boundary conditions are
 160 imposed in the spanwise direction. Finally, the flow emerges horizontally from the source with
 161 a uniform velocity profile, and the turbulence at the source is triggered by azimuthal forcing,
 162 following the approach of Zhou et al. (2001).

163 Since the study focuses on steady-state flow, the simulation duration is set sufficiently long
 164 to ensure convergence of the time-averaged statistics of the flow variables. The steady state is
 165 considered to be achieved when the variation in the mean statistical values falls below 2% of the
 166 mean value.

167 Finally, the cross-section scales of the velocity, thickness and density (respectively denoted
 168 $U(x)$, $h(x)$ and $\rho(x)$) are obtained using the following integral formulations for the mass, volume

169 and momentum fluxes per unit depth (Ellison & Turner (1959)):

$$\rho(x) U(x) h(x) = \int_0^{\infty} \varrho(x, z) u(x, z) dz, \quad (5)$$

$$U(x) h(x) = \int_0^{\infty} u(x, z) dz, \quad (6)$$

$$\rho(x) U(x)^2 h(x) = \int_0^{\infty} \varrho(x, z) u(x, z)^2 dz, \quad (7)$$

170 where $u(x, z)$ and $\varrho(x, z)$ represent the local velocity and density of the layer, respectively. For
 171 the sake of clarity, in the following, $\rho(x)$, $U(x)$ and $h(x)$ will be referred to simply as ρ , U and h
 172 respectively.

173 2.1. Longitudinal evolution of the current

174 Before examining the influence of slope on the entrainment, we first focus on the longitudinal
 175 evolution of the variables U , h and ρ , defined in the previous paragraph with the equations (5),
 176 (6) and (7), along with the Richardson number Ri for the eight cases simulated. Figure 2 shows
 177 these longitudinal evolutions for the eight cases.

178 For the case 0 ($\theta = 0^\circ$, blue lines with squares in figure 2), the simulation shows a transition.
 179 Specifically, both height and Richardson number increase until reaching a maximum at $x = 2.3m$

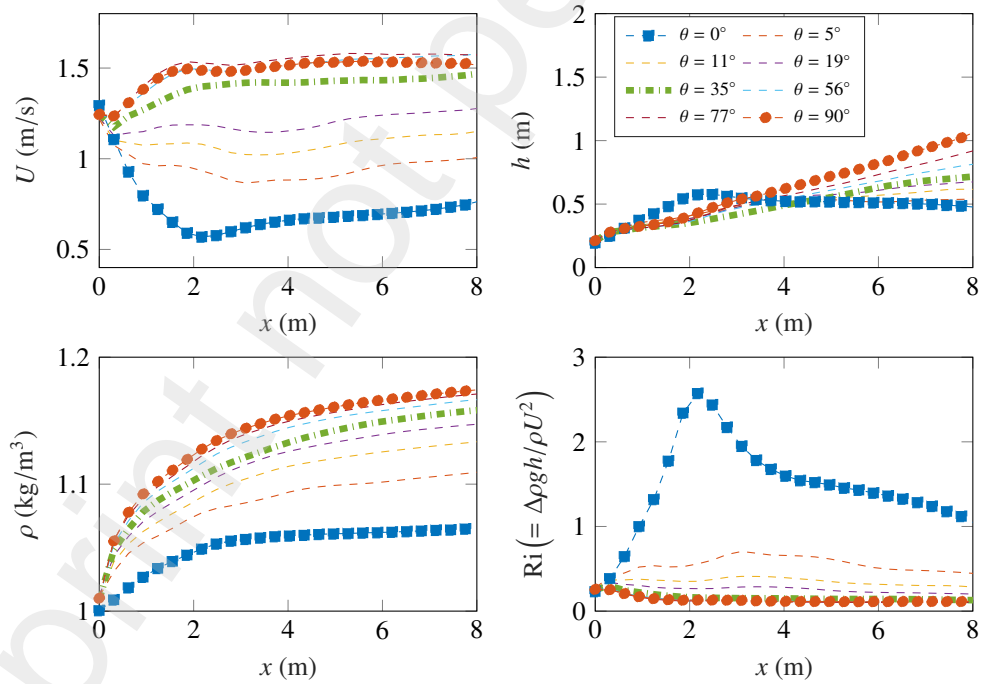


Figure 2: Longitudinal evolution of the velocity, the height, the density and the Richardson number of the flow for all the cases presented in table 2.

180 after which they decrease until the exit of the domain. The velocity also exhibits this non-
181 monotonic behavior with first a decrease and then an increase. Moreover, a transition from the
182 supercritical to the subcritical regime is observed as the Richardson number exceeds unity.

183 As the slope angle increases and reaches 5° , we notice that the Richardson number of the flow
184 does not reach unity. This indicates that there is therefore no transition associated to a change of
185 regime, although a slight non-monotonic behaviour is observed. Regarding velocity and height,
186 the former decreases initially and then stabilizes, while the latter increases continuously from the
187 injection point to the domain exit. This general behavior is consistent for all simulations with
188 slope angles below 35° (i.e. slope of 11° and 19°).

189 For angles equal or greater than 35° (green dashdotted lines in figure 2), a different behavior
190 is observed. Although the velocity decreases near the injection point, it increases rapidly and
191 stabilizes around $x = 2$ m until reaching the exit. This change, also reflected in the Richardson
192 number, suggests a new behavior where the flow gains inertia shortly after injection. These find-
193 ings are consistent with the observations of Baines (2005), who identified a transition between
194 the "gravity current" like and the "plume" like behavior for slopes in the range of $[20^\circ, 30^\circ]$. In
195 addition, for angles equal to or greater than 35° , the thickness of the current evolves linearly,
196 which is typical of plume-like flows (Michaux & Vauquelin (2008)).

197 Finally, for a 90° -degree slope (orange lines with circles in figure 2), the results show that
198 the velocity of the flow increases before reaching a constant value. The Richardson number
199 decreases slightly before stabilizing, and the height increases linearly. Additionally, the density
200 increase is most pronounced in this configuration, indicating that entrainment is greater for this
201 angle than for any of the others.

202 2.2. Study of the entrainment

203 In addition to the primary variables U , h , and ρ , the simulations also enable the computation
204 of the local entrainment coefficient E at each longitudinal position x . This coefficient is derived
205 from the mass conservation equation presented in Ellison & Turner (1959) and rewritten as:

$$E(x) = \frac{d(\rho U h)}{dx} \frac{1}{U \rho_a}, \quad (8)$$

206 From the relation (8), the evolution of the local entrainment as a function of the Richardson
207 number can be plotted, as shown in figure 3. Note that we have chosen to disregard data close
208 to the injection point ($x < 3$ m) and the outlet ($x > 7$ m) to avoid any potential influence of the
209 boundary conditions on the entrainment.

210 The analysis of figure 3 reveals, first and foremost, that the entrainment coefficient increases
211 with the slope. Specifically, each successive angle exhibits a higher entrainment than the pre-
212 ceding one. Additionally, for steeper angles (77° and 90°), the entrainment appears to remain
213 relatively constant, with values approaching 0.09, which is consistent with the value mentioned
214 in the introduction for a vertical planar wall plume.

215 Moreover, this figure shows that the entrainment becomes progressively more constant as the
216 slope increases. Finally, this figure also shows that the influence of angle strongly depends on the
217 magnitude of the angle. For small slope angles, the increase in entrainment seems to be slight,
218 whereas for larger angles, this increase is more pronounced.

219 These results confirm that entrainment is influenced by both the Richardson number and the
220 slope. At lower slope angles, the Richardson number plays a significant role, but its influence

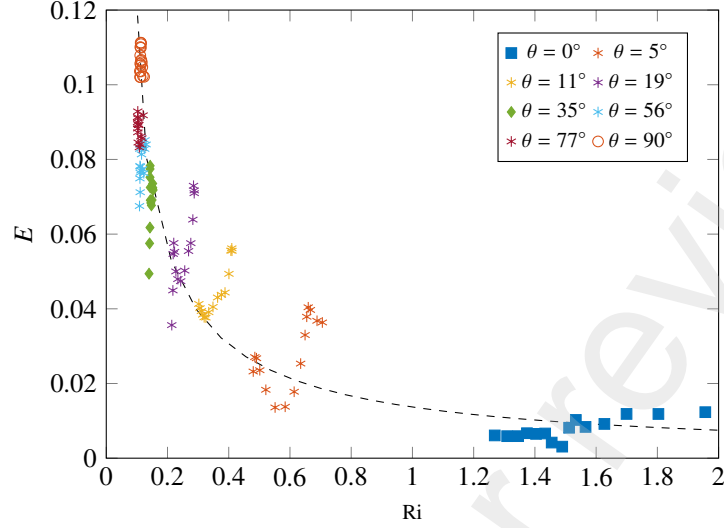


Figure 3: Evolution of the local entrainment E as a function of the Richardson number Ri for all the cases presented in table 2.

221 diminishes as the slope increases, eventually vanishing for vertical angles (90°). It is now inter-
 222 esting to focus on the theoretical aspects of the current in order to better understand the influence
 223 of the slope on the flow.

224 3. Theory

225 3.1. Governing equations

226 We consider a steady gravity current flowing along a wall of length L , inclined at an angle
 227 θ to the horizontal, as illustrated in figure 4. The current is released with a density ρ_0 at a
 228 horizontal velocity u_0 from a rectangular nozzle of thickness h_0 . The surrounding fluid, having
 229 a density $\rho_a (> \rho_0)$, is at rest. Furthermore, we assume that the flow is always supercritical at the
 230 injection, as in the simulations carried out in section 2 (i.e. $Ri_0 < 1$). The cross-section scales of
 231 the velocity, thickness and density, denoted by U , h and ρ , respectively, are obtained using the
 232 integral formulations for the mass, volume and momentum fluxes presented in equations (5), (6)
 233 and (7).

234 The governing equations of the steady gravity current are derived by considering a balance
 235 of mass, momentum and buoyancy on an infinitesimal element of length dx . These governing
 236 equations can be expressed as follows:

$$\frac{d(\rho U h)}{dx} = E U \rho_a, \quad (9)$$

$$\frac{d(\rho U^2 h)}{dx} = \Delta \rho g h \sin(\theta) - \frac{1}{2} \frac{d(\Delta \rho g h^2 \cos \theta)}{dx} - C_d \rho U^2, \quad (10)$$

$$\frac{d}{dx} \left(\frac{\Delta \rho}{\rho_a} g U h \right) = 0, \quad (11)$$

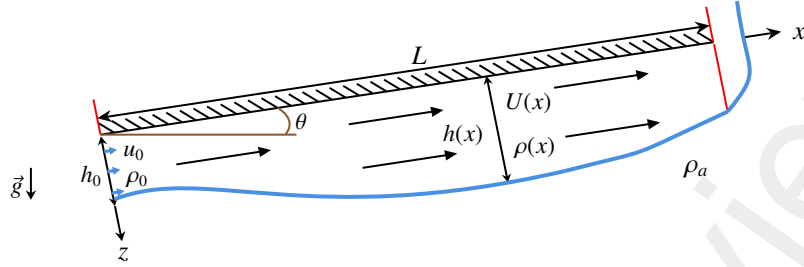


Figure 4: Schematic of the inclined gravity current configuration.

237 where E is the local entrainment coefficient and C_d represents the drag coefficient. The RHS of
 238 the equation (10) stand respectively for the buoyancy force due to the slope, the pressure force
 239 on the flow arising from variations in thickness and density and the basal drag force due to the
 240 friction between the current and the inclined wall. These ordinary differential equations can be
 241 combined to derive the longitudinal evolution of the velocity, thickness and density:

$$\frac{dU}{dx} = -\frac{U \left(\frac{\rho_a}{\rho} - \frac{1}{2} \text{Ri}_\theta \right) E + C_d - \text{Ri}_\theta \tan \theta}{h (1 - \text{Ri}_\theta)}, \quad (12)$$

$$\frac{dh}{dx} = \frac{\left(1 + \frac{\rho_a}{\rho} - \frac{1}{2} \text{Ri}_\theta \right) E + C_d - \text{Ri}_\theta \tan \theta}{1 - \text{Ri}_\theta}, \quad (13)$$

$$\frac{d\rho}{dx} = \frac{\Delta\rho E}{h}, \quad (14)$$

242 where Ri_θ is the projected Richardson number:

$$\text{Ri}_\theta = \frac{\Delta\rho h g \cos \theta}{\rho U^2} = \text{Ri} \cos \theta. \quad (15)$$

243 The evolution of Ri_θ is obtained by combining equations (12), (13), (14) and (15):

$$\frac{d\text{Ri}_\theta}{dx} = \frac{\text{Ri}_\theta \left(1 + 2 \frac{\rho_a}{\rho} \right) \left(1 + \frac{1}{2} \text{Ri}_\theta \right) E + 3 C_d - 3 \text{Ri}_\theta \tan \theta}{h (1 - \text{Ri}_\theta)}. \quad (16)$$

244 When the angle tends towards 0 in equations (12), (13), (14) and (16), we find the equations
 245 for a non-Boussinesq gravity current propagating on a horizontal wall. In this configuration,
 246 the Richardson number increases until it reaches unity, where a singularity arises. Haddad et
 247 al. (2024) proposed to introduce a discontinuity, similar to a hydraulic jump, to circumvent this
 248 issue. The location and amplitude of this jump are determined using conservation equations on
 249 either side of the discontinuity, as well as a critical boundary condition at the exit of the domain.
 250 However, as the slope increases, the mathematical singularity no longer appears. Indeed, a closer
 251 look at equations (12), (13) and (16) reveals that when the following condition is met:

$$\theta > \arctan \left[\frac{\left(1 + 2 \frac{\rho_a}{\rho} \right) \left(1 + 2 \text{Ri}_\theta \right) E + 3 C_d}{3 \text{Ri}_\theta} \right], \quad (17)$$

252 then the numerator of equations (12), (13) and (16) is not strictly positive. By replacing Ri_θ by
 253 1, it is possible to define the critical angle θ_c :

$$\theta_c = \arctan \left[\left(1 + 2 \frac{\rho_a}{\rho} \right) E + C_d \right], \quad (18)$$

254 which corresponds to the angle beyond which the singularity is never reached. Additionally, if
 255 the slope angle exceeds this critical angle, the numerator of (16) becomes zero before Ri_θ reaches
 256 unity. In this case, the flow reaches a "normal regime", as Ellison & Turner (1959) called it in
 257 their article, in which the Richardson number no longer varies. Conversely, if the slope is less
 258 than this critical angle, the mathematical singularity arises. Practically, although it depends on
 259 the ratio between the densities as well as the entrainment and drag coefficients, this angle is quite
 260 small, as specified by Britter & Linden (1980) who experimentally obtained $\theta_c = 0.5^\circ$. These
 261 findings are corroborated by the results of the LES simulations presented in section 2, where
 262 it was observed that for a 5° slope, the Richardson number no longer reaches unity and tends
 263 towards a constant value, indicating that the critical angle θ_c has been exceeded, for our source
 264 conditions.

265 Moreover, we can investigate the angle from which the normal state is achieved immediately
 266 after the injection. Referring to equation (17), and substituting Ri_θ by $Ri_\theta(x=0)$, we then find
 267 the supercritical angle θ_{sc} :

$$\theta_{sc} = \arctan \left[\frac{\left(1 + 2 \frac{\rho_a}{\rho} \right) (1 + 2 Ri_\theta(x=0)) E + 3 C_d}{3 Ri_\theta(x=0)} \right]. \quad (19)$$

268 When $\theta > \theta_{sc}$, the fluid gains in inertia and the Richardson number decreases immediately after
 269 the injection. When $\theta = \theta_{sc}$, the Richardson number remains constant from the injection to the
 270 exit of the domain. Finally, for $\theta_c < \theta < \theta_{sc}$, the Richardson number increases until the fluid
 271 reaches the normal state and remains constant. For our source conditions, it was found that the
 272 supercritical angle θ_{sc} appears to be near 35° .

273 By the way, for the particular case when $\theta = 90^\circ$, namely for the planar wall plume, equa-
 274 tions (9), (10) and (11) lead to:

$$\frac{d(\rho U h)}{dx} = E U \rho_a, \quad (20)$$

$$\frac{d(\rho U^2 h)}{dx} = \Delta \rho g h - C_d \rho U^2, \quad (21)$$

$$\frac{d}{dx} \left(\frac{\Delta \rho}{\rho_a} g U h \right) = 0. \quad (22)$$

275 These equations correspond to those presented by Parker et al. (2020) but extended to the non-
 276 Boussinesq configuration. For this slope, the entrainment coefficient E is constant (≈ 0.09).

277 3.2. A generalized entrainment coefficient ?

278 Given that above observations show that both the Richardson number and the slope angle
 279 influence the entrainment, we propose to include these two parameters in a new entrainment law.
 280 This model must satisfy three conditions:

- 281 • The law depends only on the Richardson number when the slope angle is null.

- 282 • The law is constant when the slope angle is 90° .
- 283 • The influence of the planar wall plume must be greater than the influence of the gravity
- 284 current.

285 On the basis of these considerations and from the results of the literature introduced in section 1,
 286 we propose to combine the law of Christodoulou (1986), valid for a range of $Ri \in [0.1, 10]$,
 287 with the observations from the LES simulations and for the vertical planar wall plume in order
 288 to write:

$$E(\theta, Ri) = \frac{0.002}{Ri} \cos \theta + 0.09 \sin^{1/2} \theta. \quad (23)$$

289 The coefficient $1/2$ on the sinus term is intended to represent the transition from the gravity flow
 290 behaviour to the planar wall plume behaviour mentioned in the third condition above. This is in
 291 agreement with the results of Baines (2005), who suggest that the "plume" behaviour manifests
 292 before the "gravity current" behaviour disappears.

293 4. Comparison between the theoretical model and the numerical simulations

294 We can now test the reliability and robustness of the generalized entrainment model (23) by
 295 comparing the results of the LES simulations with those of the theoretical model (equations (12),
 296 (13) and (14)). The model requires also a value for the drag coefficient, and we adopt the value
 297 $C_d = 0.0065$ as prescribed in Kunsch (1998). This coefficient corresponds to a flow of hot air
 298 into an ambient environment and has been used in similar studies, such as Hu et al. (2005), Chow
 299 et al. (2015), Chow et al. (2016) and Haddad et al. (2022).

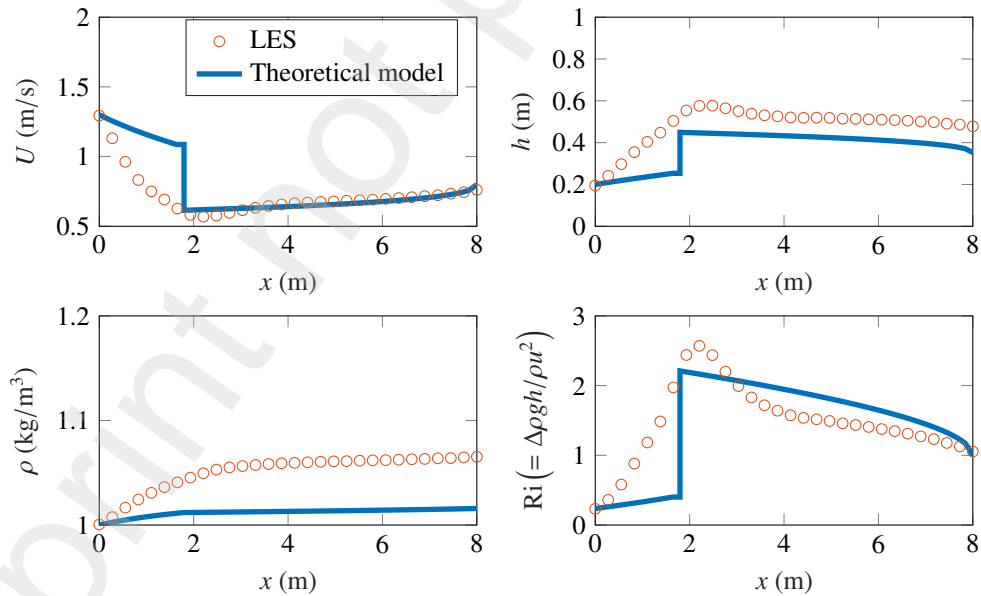


Figure 5: Longitudinal evolution of the velocity, the height, the density and the Richardson number of the flow for the case 0 ($\theta = 0^\circ$). The red circles correspond to LES simulation and the blue lines correspond to the solution given by theoretical model.

300 In the no-slope configuration (case 0, $\theta = 0^\circ$), a straightforward numerical resolution with the
 301 theoretical model is not achievable. As discussed in section 2.1, the flow exhibits non-monotonic
 302 behaviour, and the Richardson number exceeds unity, leading to the appearance of a singularity
 303 during the solving. To circumvent this issue, we used the hydraulic jump without entrainment.
 304 Further details of the solution method can be found in the work of Haddad et al. (2022), but
 305 briefly the method consists in applying the Bélanger (or Rankine-Hugoniot) equations before
 306 reaching the singularity to jump from a Richardson number below unity to a Richardson number
 307 above unity. The location of the jump is then defined by imposing $Ri = 1$ at the exit of the
 308 domain, as in the hydraulic configuration (Henderson (1966), Chanson (2004)). Hence, the
 309 solution satisfies the conservation equations for the supercritical phase, the Bélanger equations
 310 for the regime transition, the conservation equations for the sub-critical phase (after the jump)
 311 and critical Richardson number at the exit of the domain.

312 Comparisons between the model and the LES simulation for the velocity, the height, the
 313 density and the Richardson number of the current are displayed in figure 5. This figure shows
 314 that the theoretical model, incorporating the jump, reproduces the non-monotonic behavior of the
 315 flow. From a quantitative point of view, the theoretical model provides a reliable estimation of U ,
 316 h and ρ on both side of the discontinuity, although it slightly underestimates the thickness. The
 317 primary source of discrepancy lies in the abrupt nature of the hydraulic jump in the model, which
 318 is more gradual in the simulation. Regarding the density, the model exhibits similar behaviour
 319 with a relative error of less than 5%, indicating that the selected entrainment law is appropriate
 320 for this type of flow.

321 In the case with a slope, we compare the theoretical results obtained using the entrainment

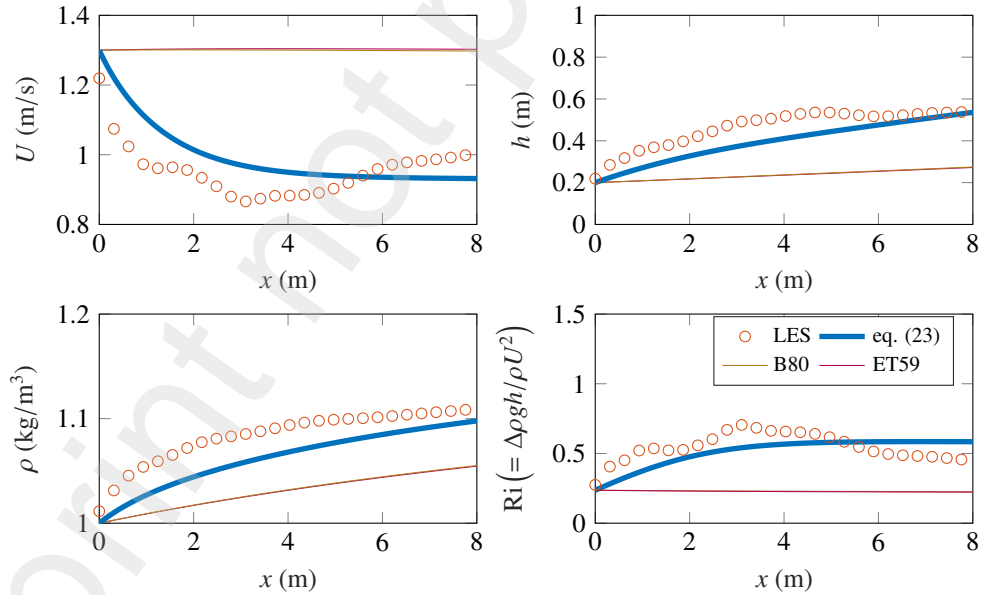


Figure 6: Longitudinal evolution of the velocity, the height, the density and the Richardson number of the flow for the case 1 ($\theta = 5^\circ$). The red circles correspond to the LES simulation. The theoretical results are obtained by successively using the entrainment law given by equation (23) as well as the laws of Hopfinger (1983) based on the results of Ellison & Turner (1959) (ET59) and Briggs (1980) (B80).

322 law (23) with the theoretical results obtained using the law established by Briggs (1980) (see
 323 table 1) and the law of Hopfinger (1983) derived from the data of Ellison & Turner (1959).
 324 The results obtained with the LES simulation and with the theoretical model for these different
 325 laws on a weak slope (5°) are shown in figure 6. It becomes apparent that the entrainment laws
 326 from the literature fail to accurately represent the flow, resulting in relative errors in the primary
 327 quantities on the order of 50%. These laws seem inadequate to capture the behavior of the flow
 328 with an almost constant velocity and Richardson number on the whole domain, whereas the
 329 simulation clearly shows an increase and a decrease, respectively. This suggests that a global
 330 approach is not well-suited for modeling such flows under these conditions. On the contrary,
 331 when applying the entrainment law given by relation (23), the model provides more accurate
 332 results, both qualitatively and quantitatively, for all the variables calculated. This is especially
 333 true for the density, which suggests that the entrainment is more conveniently represented by the
 334 newly built relation (23). Nevertheless, even if our model cannot reproduce some slight non-
 335 monotonic local behaviours observed in the LES simulation (near the injection and the outlet), it
 336 gives an acceptable estimation of these quantities over a large section of the domain.

337 The same graphs can be plotted with an intermediate slope (35°) (figure7). In this case, the
 338 entrainment laws from the literature yield better results than in the previous configuration, but
 339 the relation (23) provides again better results, with relative errors on height and density of less
 340 than 8% and 5%, respectively.

341 For a steeper slope ($\theta = 77^\circ$), the results are displayed in figure 8. This time, the law of Briggs
 342 (1980) provides the least satisfactory results. The law of Hopfinger (1983), based on the results of
 343 Ellison & Turner (1959), offers results that are reasonably consistent with the LES simulation, in

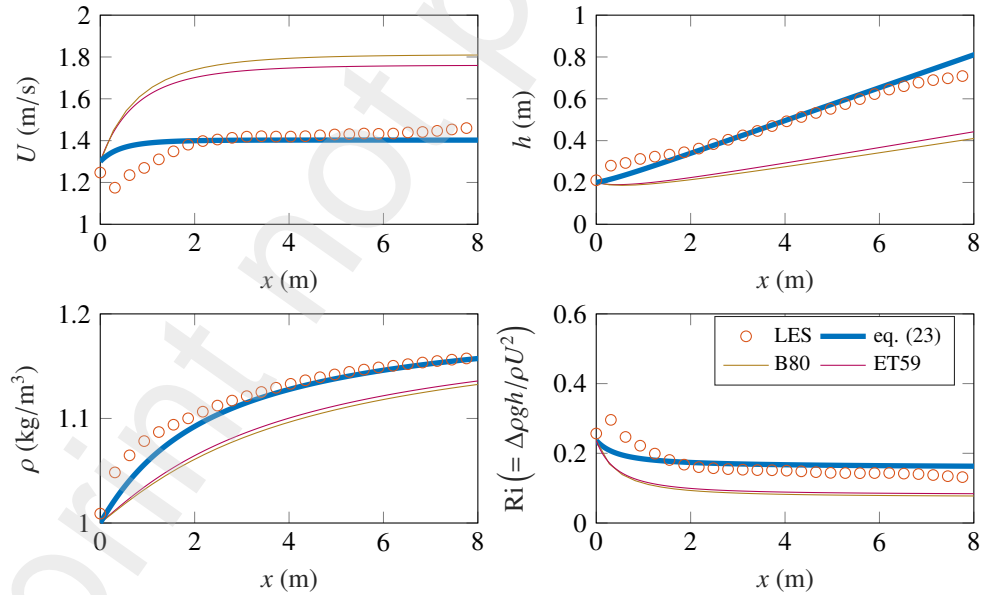


Figure 7: Evolution of the velocity, the height, the density and the Richardson number of the flow for the case 4 ($\theta = 35^\circ$). The red circles correspond to the LES simulation. The theoretical results are obtained by successively using the entrainment law given by equation (23) as well as the laws of Hopfinger (1983) based on the results of Ellison & Turner (1959) (ET59) and Briggs (1980) (B80).

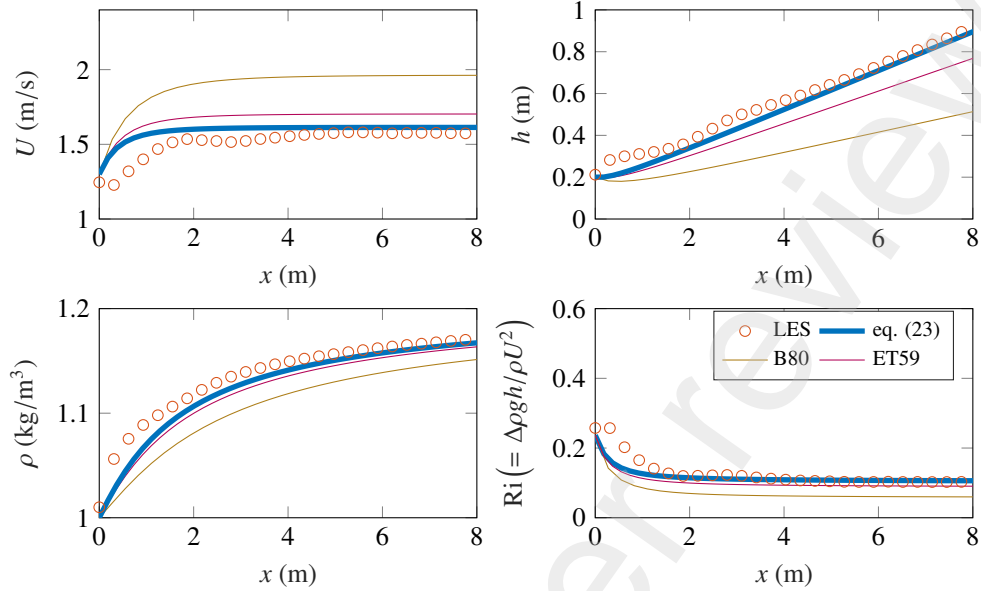


Figure 8: Evolution of the velocity, the height, the density and the Richardson number of the flow for the case 6 ($\theta = 77^\circ$). The red circles correspond to the LES simulation. The theoretical results are obtained by successively using the entrainment law given by equation (23) as well as the laws of Hopfinger (1983) based on the results of Ellison & Turner (1959) (ET59) and Briggs (1980) (B80).

344 line with its intended application for angles approaching 90° . Our law remains close to the LES
 345 simulation results, with an average relative error of 15% across the entire domain. Furthermore,
 346 this error is higher near the left boundary due to injection effects. Excluding this near-source
 347 region of limited spatial extent, the relative error decreases to below 10%.

348 Finally, and for illustrative purposes, we test the performance of our model in the planar
 349 wall plume configuration (i.e. with an angle of 90°). These results are presented in figure 9.
 350 The model provides a reliable prediction of the main variables (U , h and ρ) and the Richardson
 351 number, confirming its suitability even in this extreme configuration.

352 5. Conclusions

353 In this article, we investigated a miscible, steady, two-dimensional gravity current flowing
 354 along an inclined boundary. We focused on the evolution of its dynamics, of the entrainment
 355 coefficient E and on its dependence on both the slope and Richardson number.

356 To achieve this, we carried out eight large-eddy simulations, maintaining the injection con-
 357 ditions while varying the slope angle to cover a range from 0 to 90° . First, these simulations
 358 enabled us to observe the longitudinal evolution of the cross-section scales of velocity U , density
 359 ρ and height h of the current, as well as the Richardson number Ri , corresponding to the ratio
 360 between the buoyancy and inertial forces.

361 From these simulations, three distinct scenarios emerged. In the absence of slope (i.e.,
 362 $\theta = 0^\circ$), the velocity and height exhibited a non-monotonic behaviour, with velocity decreasing
 363 initially, followed by an increase, and an opposite trend for the thickness. The Richardson

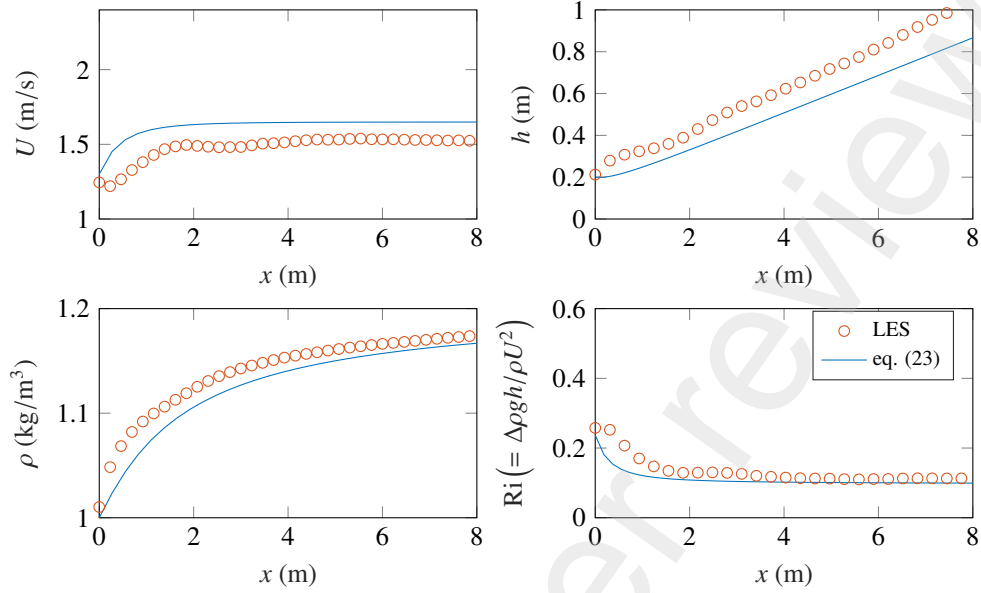


Figure 9: Evolution of the velocity, the height, the density and the Richardson number of the flow for the case 7 ($\theta = 90^\circ$). The red circles correspond to the LES simulation and the blue lines corresponds to the model with the equation (23).

364 number displayed similar non-monotonic behaviour, increasing until it exceeds unity, then de-
 365 creasing until the end of the domain. This indicated a flow transition from a supercritical to a
 366 subcritical regime. As the slope increased (between 5° and 35° according to our simulations),
 367 the flow showed a second regime characterized by an increasing Richardson number that stabi-
 368 lized at a value always below unity. In addition, both U and h displayed monotonic behavior,
 369 stabilizing toward the end of the domain. Finally, for angles exceeding 35° , we observed a third
 370 scenario in which the Richardson number decreased immediately after injection before stabi-
 371 lizing. In this configuration, the flow velocity increased from the injection point, gaining inertia in
 372 the streamwise direction.

373 Secondly, these simulations also enabled us to extract the local entrainment E . We noted
 374 a gradual increase of E with increasing slope angle, reaching a nearly constant value for a 90°
 375 angle. These findings are consistent with the existing literature for the two extreme cases ($\theta = 0^\circ$
 376 and $\theta = 90^\circ$), with a dependence between the Richardson number and the entrainment for small
 377 angles and a constant entrainment coefficient for angles equal to or close to 90° . We develop
 378 a new entrainment model that includes both the influence of the Richardson number and the
 379 inclination. By combining the law of Christodoulou (1986) and data observed in the literature
 380 for a planar wall plume (Ellison & Turner (1959), Grella & Faeth (1975), Parker et al. (2020)),
 381 we proposed the law $E = 0.002 \cos(\theta)/\text{Ri} + 0.09 \sin^{1/2}(\theta)$. This law unifies the entrainment of a
 382 gravity current with the entrainment of a planar wall plume.

383 In conjunction with the numerical study, we also examined the theoretical aspect of gravity
 384 currents. Our modeling was grounded in the work of Ellison & Turner (1959) and extended
 385 within the non-Boussinesq framework. This model, based on the equations of conservation of
 386 mass, momentum and buoyancy, allows the longitudinal evolution of velocity, thickness, density
 387 and Richardson number to be calculated. This model depends on the entrainment coefficient E

388 and exhibits a mathematical singularity when the Richardson number is equal to 1.

389 Following a mathematical analysis of the model, we analytically identified two specific an-
390 gles: the critical angle θ_c and the supercritical angle θ_{sc} . The critical angle corresponds to the
391 angle beyond which the mathematical singularity no longer exists. Consequently, for angles
392 greater than θ_c , there is no mathematical difficulties in solving the equations. For its part, the
393 supercritical θ_{sc} angle corresponds to the angle above which the Richardson number of the flow
394 decreases immediately after the injection. In this configuration, the flow acquires inertia as it
395 flows. These two angles were corroborated through LES simulations, with approximate values
396 of 5° for θ_c and 35° for θ_{sc} .

397 Lastly, we employed our theoretical model with the proposed entrainment law and compared
398 the results with those from models found in the literature. For each scenario identified (and
399 illustrated respectively by the angles $\theta = 5^\circ$, $\theta = 35^\circ$ and $\theta = 77^\circ$), our model provides better
400 predictions than the laws from the literature. We also ran simulations at the two extreme cases,
401 namely, 0° and 90° to confirm the model in the gravity current and in the planar wall plume
402 configuration and the resolution of the theoretical model using the new entrainment law again
403 provided results close to those obtained by LES simulation.

404 The newly developed entrainment law thus enhances the representativeness of the model
405 proposed by Ellison & Turner (1959) across a range of angles from 0° to 90° . However, it is
406 important to note that this model does not encompass all ranges of Richardson numbers. Specif-
407 ically, the law presented by Christodoulou (1986) is only applicable for the range $Ri \in [0.1, 10]$.
408 For flows exhibiting more inertial or buoyant characteristics, it would be beneficial to modify
409 the "gravity current" contribution of the entrainment law to ensure consistency with the existing
410 literature.

411 6. Declaration of interests

412 The authors declare that they have no known competing financial interests or personal rela-
413 tionships that could have appeared to influence the work reported in this paper.

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